

Amendment to the Specification:

Page 1, below the title and above "Field of the Invention", please insert the following new paragraph:

--This application is the United States national phase application of International Application PCT/JP2004/004317 filed March 26, 2004.--

Please replace the paragraph starting on page 38, line 36 through page 40, line 11 with the following amended paragraph:

In liquid medium recovery system 10 according to one embodiment of the present invention shown in ~~Fig. 1~~ Fig. 3, 100 mL of an ethanol-containing material, which had been used as an eluent for chromatography, was led to closed tank for solvent feeding 50, and the recovered organic solvent was fed dropwise to the closed system from recovered solvent feed inlet 24 using pressure-vacuum dual pump P-2 at a feed rate of 34 mL/min. Diaphragm pump P-1 was controlled so that the gas (air) flow rate became 6 L/min, and the gas was passed through conduit 60 (outer diameter: 6 mm; inner diameter: 4 mm), and conduit 60 was arranged so that the tip of conduit 60 fixed by branch pipe 36 was positioned 6 cm above the bottom of distilling round-bottom flask receiver 26 having a capacity of 1 L. The gas was blown through conduit 60 obliquely

against the surface of the recovered organic solvent so that a depressed round area about 2 to 4 mm in depth was formed in the surface of 3 to 4 cm of the recovered organic solvent collected in distilling round-bottom flask receiver 26. The gas blown to the bottom of distilling round-bottom flask receiver 26 moved upwards in the flask, together with the vaporized ethanol, and then arrived at heating portion 22. Heating portion 22 has a straight-pipe distilling portion (inner diameter: 60 mm; length: about 200 mm), and a spiral pipe comprised of a pipe having an outer diameter of 8 mm disposed in the distilling portion, wherein the spiral pipe has a helix outer diameter of 55 mm. A heating bath medium was fed from heating bath 40 into the pipe of the spiral pipe by means of heating bath circulation pump P-3, and the heating bath medium was made to circulate between heating bath 40 and heating portion 22 comprising the spiral pipe to keep heating bath 40 and heating portion 22 at 65°C. Thus, the recovered solvent fed dropwise from recovered solvent feed inlet 24 moved downwards along and in contact with the outer surface of the spiral pipe and the inner wall of the straight-pipe distilling portion in heating portion 22, and brought to contact with the gas flowing upwards in the heating portion, so that part of the recovered

solvent was vaporized. The ethanol vaporized in both the distilling round-bottom flask receiver and heating portion 22 passed through connecting conduit 70 and then arrived at cooling condenser for condensing 102 where the ethanol was cooled and condensed into liquid, so that the ethanol liquid was gradually collected in round-bottom flask receiver 104 having a capacity of 1 L. Under the above conditions, almost all the ethanol (>99%) was recovered in round-bottom flask receiver 104 at a rate of about 8.5 mL/min.